



# Article **Densification and Fuel Properties of Onion Husks**

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**Abstract:** The aim of the described research was to assess the suitability of onion husk waste as a material for the production of solid fuels in the form of granules (pellets). Due to the low susceptibility to thickening of onion husks, the addition of a binder in the form of potato pulp was used (waste with a high starch content). Both wastes were subjected to elemental analysis determining the content of C, H, N, S, Cl, and their HHV (High Heating Value) and LHV (Low Heating Value). Mixtures containing the addition of 10%, 15%, and 20% potato pulp to onion husks were subjected to granulation in a "flat matrix–thickening rollers" operating system at three rotational speeds of the granulator matrix a 170, 220, and 270 rpm. The influence of the potato pulp addition and matrix rotational speed on the quality of the obtained pellet was determined. The highest quality product was combusted in a low-power boiler with a retort grate, and the content of CO, CO<sub>2</sub>, SO<sub>2</sub>, NO, and HCl in the exhaust gas was determined. The highest quality granulate was obtained from a mixture containing 10% potato pulp, which was compacted at 170 rpm matrix, where the kinetic strength was 99.50% and the density was about 650 k·gm<sup>-3</sup>. The results of the combustion emissions from onion husk granules exceed the requirements of the EcoDesign Directive with the greatest being the case of CO.

Keywords: onion husks; potato pulp; densification; combustion; emission

# 1. Introduction

In recent years, biomass, including waste biomass (bio-waste) from the agri-food industry, has increasingly been used as a raw material for heat and electricity production due to the commonly observed requirement to reduce carbon dioxide emissions [1].

Bio-waste is food and kitchen waste from caterers, households, commercial premises, and food processing plants [2]. Every month, millions of tons of these kinds of bio-waste are produced. Some are allocated to landfills, and some are exported to third world countries. This has a serious impact on the environment, human health, and wildlife. For this reason, many new processes for the generation of energy from waste are constantly being developed [3–8].

One of the raw waste materials generated in vegetable processing plants is post-production onion waste. According to the Polish Act on waste of 27 April 2001 [9], onion husk was in group 02 (waste from agriculture, horticulture, hydroponics, fishing, forestry, hunting, and food processing), with code 02 03 80 (pomace, sediments, and other wastes from the processing of plant products).

According to Benitez et al. [10], waste from onion processing is mainly onion husks (skins), i.e., two outer fleshy scales (skins) and roots removed from the vegetable during industrial peeling as well damaged or undersized malformed bulbs. Waldron [11] considered these wastes as an environmental

problem. Onion waste, because of its characteristic aroma, is unsuitable in high concentrations for fodder nor as an inorganic fertilizer because of the rapid development of phytogenetic agents.

Ly and co-workers [12] reported that the dry outer skins of onion contain high contents of quercetin, quercetin glycoside, and their oxidative products, which may be effective antioxidants against non-enzymatic lipid oxidation. Many studies have confirmed that different parts of the onion bulb may serve as promising sources of natural antioxidants [13,14]. On the other hand, Benitez and co-workers [10] found that onion composition is variable and depends on the bulb section cultivar, environment, maturation stage, and storage time. Therefore, it is necessary to study the composition of each part to know its potential purposes.

Solid waste of agri-food origins can be submitted to a densification (agglomeration) process, where the material obtains a permanent geometric form of a granulate (agglomerate, pellet) or briquette due to external and internal forces [15]. The granulation process (agglomeration, densification) of waste materials favors their transport and storage (increase of bulk density) and allows their application in installations with automatic fuel feeding systems. Moreover, through the process of densification, it is possible to obtain a product that is a mix of a few components, which allows modeling of the required properties of the produced fuel [16].

Ohman and colleagues [17] stated that the quality of biomass pellets can be improved by the addition of a hydrolytic post-production waste, resulting from the production of ethanol from lignocellulose. As a result of the addition, the heating value of pellets increased, and the ash content decreased. Miranda and colleagues [18], who compacted olive waste pulp (a by-product of olive oil production), found that the addition of Pyrenean oak waste to the olive pulp ensured a more effective compacting of the mixture, improved the kinetic durability of the obtained granulate, and reduced its ash content. Chou et al. [19,20], in searching for the optimal conditions for obtaining fuel briquettes from rice waste (straw and bran), found that along with the increase of rice bran in the compacted mixture, the strength of the briquette and its calorific value increased in the process of densification in a piston-matrix system.

Celma and colleagues [21] investigated the granulate from industrial post-production tomato waste (skins and seed cores), concluding that its hardness and kinetic durability depends on the moisture of the used biomass, as well as on further activities related to the reduction of its humidity after compaction and the storage time of the obtained granulate. Stahl and Berghel [22] determined that with the increase in the turnip waste content in the compacted mixture with sawdust, the mechanical strength and density of the obtained granulate, as well as the energy consumption of the agglomeration process, were decreased. Sotannde and colleagues [23], in examining the effect of binder addition (arabic gum and cassava starch) in the process of charred (torrified) wood waste briquetting, stated that the use of both binder materials allowed high-quality briquettes (high kinetic durability and calorific value) to be obtained.

One of the post-production wastes generated from agri-food processing plants is buckwheat husk. According to Chachułowa and colleagues [24], buckwheat husk can be used as an additive to animal feed, which may be stored longer. However, according to Chachułowa and co-workers [24], the low bulk density of the husk impedes its transport, so processing at the plants in which it is produced is required. The tests conducted by the authors of this paper allowed for the conclusion that raw buckwheat husk is a material with low susceptibility to densification. Based on the tests, it was found that buckwheat husk has a low moisture content of approximately 8.4% and low bulk density of about 186 kg·m<sup>-3</sup>. Pressure agglomeration of husks with such low humidity gives unsatisfactory results. In order to increase its susceptibility to compaction and to obtain high-density granules, some pretreatments should be done, for example, increased humidity or a binder additive. Potato pulp can be such an addition, as demonstrated by earlier authors' research [25–27].

Undertaking research related to post-harvest waste management allows public awareness of the use of agricultural waste as energy sources to be raised, and also shows a specific example of how to

convert waste biomass into fuel. The use of onion husk residue for fuel purposes is not a topic that is often discussed by researchers dealing with this waste.

According to earlier research of compacting post-production onion waste carried out by the authors [28], onion waste is a material characterized by a small susceptibility to densification. During pelleting, a high process temperature is required in order to obtain pellets with satisfactory quality parameters. An increased moisture content in the densified onion waste has a significant impact on the pelleting process and the quality of the obtained pellets. The authors [28] found that increasing the moisture content of the densified onion waste from 17.1% to 24% resulted in a decreased energy consumption of the pelleting device by approximately 22.6% (from 2.61 to 2.02 kW) and a simultaneous reduction in the pellets' density by approximately 14.8% (from 1280.48 to 1090.29 kg·m<sup>-3</sup>) and a slight reduction in the kinetic durability of pellets by approximately 0.5% (from 97.80% to 97.24%).

A continuation of the above tests is presented in this work, where the impact of a binder addition in the form of potato pulp on the compaction process of onion husks was determined. The mechanical and fuel properties of the obtained granulate, as well as studies of the effects of its combustion, were tested to provide answers on its usefulness for energy purposes.

The purpose of the work was to analyze (based on research results) the fuel suitability of onion waste. The aim of the work was to determine the impact of material and process parameters on the energy consumption of the granulation process and on the quality of the obtained granulate (density and kinetic durability), its elementary analysis, heat of combustion, and calorific value as well as to determine the effects of combustion of the obtained granulate.

#### 2. Materials and Methods

#### 2.1. Materials

The paper presents the results of research on the granulation process of ground onion waste (Figure 1) obtained from the peeling onion plant located in Meho for the needs of the P.P.H.U (Production, Service and Trade Enterprise) cold store Eldom Grudziadz.



(a) Figure 1. Cont.



(c)

**Figure 1.** Post-production onion waste: (**a**) during drying in ambient conditions, (**b**) after drying, (**c**) in crushed and dried form own photograph.

Pre-drying of the obtained post-production waste was carried out in atmospheric conditions by means of free convection. The collected raw material was loosely distributed in field conditions (Figure 1a). Pre-dried onion waste (Figure 1b) was ground to a particle size of approximately 5 mm and smaller (Figure 1c) using a "Bak" H-111 flail shredder equipped with 5 mm sieves.

## 2.2. Methods

#### 2.2.1. Physicochemical Properties of the Raw Materials

Determination of the granulometric distribution of shredded onion husk waste was carried out in accordance with [29,30], using a LPz-2e laboratory shaker from Multiserv Morek company, equipped with a set of sieves with a mesh diameter of 6, 5, 4, 3.15, 2, 1.6, 1, 0.5, 0.25, 0.125, and 0.063 mm. Each time, a sample of 100 g of the raw material was dosed into the upper sieve and the shaker was activated for 5 min. After this time, the residue that was on each of the sieves was weighed on an analytical balance. The analysis was repeated three times. The result was an arithmetic average of the tests.

Before the pressure agglomeration process, the material's (onion husk) moisture content was tested in accordance with [31], using a WPE 300S moisture analyzer with an accuracy of 0.01%. The moisture content of five samples weighing approximately 5 g each was determined. The average of the obtained results was taken as the final result of the moisture determination. The bulk density of tested materials was analyzed in accordance with [32].

The content of C, H, N, and S were determined using the LECO CHN628 elementary analyzer in accordance with [16,33,34]. The chlorine content in the onion husks and potato pulp was determined using the S2 PICOFOX fluorescence spectrometer under the method given by the manufacturer. Analysis of the volatile parts content (according to [35,36]), moisture content (according to [36]), and ash content (according to [37]) in the onion husks and potato pulp was carried out on the LECO TGA-701 analyzer. The heat of combustion (HHV) was tested in accordance with [38] using the Kl-12Mn calorimeter. The calculations of the low heating value (LHV) were based on the material moisture and hydrogen content.

#### 2.2.2. Pressure Agglomeration Process

Tests of the pressure agglomeration process (granulation) were carried out at the SS-4 laboratory stand (Figure 2), in which the main element is a P-300 granulator with a flat matrix, as described in previous works [16,27].



**Figure 2.** View of the laboratory stand SS-4: (**a**) scheme: 1—working system of the granulator, 2—electric motor (Y132M, 7.5 kW, 1440 obr·min<sup>-1</sup>), 3—raw material feed, 4—spill granulate, 5—vibrating dispenser (FRITISCH LABORET 24), 6—power demand universal meter (METROL KWS 1083, max 20 kW, 7—Spider 8 recorder, 8—computer, (**b**) view of SS-4.

Densification tests of the onion husks and potato pulp mixture were carried out with the following input parameters:

 $x_1 = z_w$ —potato pulp content (10%, 15% and 20%) and

 $x_2 = n_m$ —granulator matrix rotational speed (170, 220 and 279 rpm).

The granulators matrix holes were 6 mm in diameter and 28 mm in length. The mass flow rate of the raw material mixtures through the granulator working system was set for all tests at the level of approximately 50 kg·h<sup>-1</sup>.

The kinetic durability of the obtained pellets was tested according to [39] by the Holmen method. The density of pellets was determined as the ratio of the mass and volume of 10 randomly selected granules.

2.2.3. Combustion of Pellets

Combustion in a low power boiler (25 kW) with a rotary grate (Figure 3) was carried out in order to verify the emissions of the produced pellets. The laboratory stand was described in previous papers [40,41].



**Figure 3.** Low Emission Combustion Technologies laboratory stand: 1—Moderator Unica VentoEko 25 kW boiler, 2—controller of the boiler, 3—fuel tank, 4—exhaust sampling place, 5—MCA10 analyzer, 6—Microsoft tablet for archiving obtained measurement results.

The laboratory station includes a Moderator (Hajnówka) Unica VentoEko boiler and Dr. Födisch MCA10 flue gas analyzer.

In the combustion tests, pellet samples of approximately 10 kg were dosed into the boiler by an automatically controlled screw feeder. The pellet mass flow and the airflow were set by a controller in the so-called automatic Fuzzy Logic mode. The combusted fuel mass flow was constant at  $3.2 \text{ kg} \cdot \text{h}^{-1}$ . After obtaining stable combustion conditions, the boiler controller may change the mass and air flow to a small extent, which was negligible for the planned experiment.

The contents of  $CO_2$ , CO, NO, and  $SO_2$  in the flue gases were normalized to the 10% content of oxygen  $O_2$  in accordance to the formula [37]:

$$Z_{s2} = \frac{21 - O_2'}{\left(21 - O_2''\right)} \cdot Z_{s1} \left[\%, \text{ mg·m}^{-3}\right], \tag{1}$$

where:

 $Z_{s1}$ —the actual compound content in the exhaust gas [%, mg·Nm<sup>-3</sup>];

 $Z_{s2}$ —content of the compound in the exhaust gas for the calculated concentration of oxygen [%, mg·Nm<sup>-3</sup>];

*O*<sub>2</sub>—set oxygen content in the exhaust [%]; and

 $O_2''$ —actual (obtained) oxygen content in the exhaust gas [%].

The excess air factor,  $\lambda$ , was computed based on the formula used for technical calculations:

$$\lambda = \frac{21.5}{21.5 - O_2''} \quad [-]. \tag{2}$$

# 3. Results and Discussion

## 3.1. Physicochemical Properties of Raw Materials

Table 1 presents the elemental composition, moisture content, volatile matter content, and ash content in onion husks and potato pulp.

Property	Onion Husks	Potato Pulp
Moisture [%] <i>wb</i>	$9.45 \pm 0.26$	$90.11 \pm 0.12$
Bulk density [kg⋅m <sup>-3</sup> ] <i>wb</i>	$159.40 \pm 7.34$	$521.24 \pm 1.87$
Volative matter [%] <i>db</i>	$62.11 \pm 0.42$	$68.44 \pm 0.55$
Ash [%] <i>db</i>	$19.80 \pm 0.38$	$12.19 \pm 0.24$
Carbon [%] <i>db</i>	$30.60 \pm 0.46$	$41.27\pm0.56$
Hydrogen [%] db	$3.85 \pm 0.01$	$5.36 \pm 0.02$
Nitrogen [%] db	$1.00 \pm 0.00$	$0.88 \pm 0.00$
Sulphur [%] db	$0.499 \pm 0.001$	$0.441 \pm 0.002$
Chlorine [%] <i>db</i>	0.025	0.013
Oxygen <sup>1</sup> [%] <i>db</i>	64.03	47.96
HHV $[MJ \cdot kg^{-1}] wb$	$12.077 \pm 0.10$	$2.503 \pm 0.059^{\ 2}$
LHV $[MJ \cdot kg^{-1}] wb$	10.491	0.242
<b>0</b> -		

Table 1. Onion husks and potato pulp.

<sup>1</sup> By difference, <sup>2</sup> calculated by the method described in [25].

Biomass, when compared to hard coal, shows much greater variability of physical and energy parameters [42]. Compared to hard coal, solid biomass contains less elemental carbon; more oxygen, silicon, and potassium; less aluminum and iron; and has a lower calorific value and lower density [43].

In addition to the chemical composition of biomass, which has a direct impact on the effects of its combustion [40,44], the moisture and ash content are the decisive properties for the use of biomass [45]. The high moisture contents of fuel have adverse effects on the combustion process, causing a decrease in the combustion temperature and making the combustion of fuels more difficult. The effect of this is an increase in the boiler outlet loss and a decrease in its efficiency [46]. The use of raw potato pulp as an independent fuel in combustion processes is significantly hampered by its high moisture content. Thus, it is a material that may be used in the form of a small additive in combustion installations.

Carbon, hydrogen, and oxygen are the main components of solid biofuels. During combustion, carbon and hydrogen, through exothermic reactions, are oxidized to carbon dioxide  $CO_2$  and water vapor  $H_2O$ , so their content has a positive effect on the heat of combustion of biofuels. The content of oxygen is a ballast in the combustion processes [47]. There are large differences between the carbon content of different types of biomass. According to Saidur et al. [48], wood-based materials are richer in carbon than herbaceous biomass (stems, leaves, straw, scales), hence they are characterized by higher values of heat of combustion.

The authors used a simplification by calculating the oxygen content as a difference from the content of other elements in the tested materials. However, it should be noted that in the case of onions,

due to their specific layered structure, the presence of silicon compounds, resulting from inaccurate waste treatment, is also possible. These inclusions can also cause a high ash content in onion skins (so-called secondary ash).

An increase in the potato pulp content from 10% to 20% in the mixture with onion husks caused a decrease in the LHV by approximately 10.7% (Figure 4). Kriżan et al. [49] produced briquettes and pellets of various diameters from maize straw and woody biomass. Their experiment showed that a calorific value of 6-mm diameter pellets ranged from 16.99 to 17.80 MJ·kg<sup>-1</sup>. The calorific value of 8-mm diameter pellets ranged from 16.63 to 17.20 MJ·kg<sup>-1</sup>. Nevertheless, the corresponding calorific value of briquettes ranged from 14.99 to 15.66 MJ·kg<sup>-1</sup>. Additionally, the analysis showed that the ash content was also affected by the pellet diameter. The ash content of 6-mm diameter pellets was observed as 4.9% of the total volume while 8-mm diameter pellets was 5.5%.



Figure 4. LHV of cherry stones granules on the content of rye bran.

The decrease in the LHV (Figure 4) is due to onion husks having a higher calorific value than potato pulp. Zając and Szyszlak-Bargłowicz [48], using the addition of rye bran for safflower mallow, also noticed a decrease in the calorific value of the irobtained pellets. According to Obidziński and colleagues [50], the use of a binder in the form of potato pulp in a mixture with buckwheat husk also caused a decrease in the calorific value of the granulate.

A one-factor analysis of variance (one-dimensional Kolmogorov–Smirnov significance test) at the significance level of  $\alpha = 0.05$  indicated significant differences between the calorific value of the granulate obtained with the increasing content of potato pulp in a mixture with onion husk.

Figure 5 presents the particle size distribution of onion husks before the pressure agglomeration process.



Figure 5. Onion grain size composition.

According to Zawiślak et al. [51], materials with a particle size from 0.4 to 2 mm are most suitable for granulation. Research carried out by Castellano et al. [52] showed a reduction in the energy consumption of pelleting along with a reduction of the particle size of wood and non-wood materials from 4 to 2 mm.

#### 3.2. Pressure Agglomeration Process

The influence of process and material factors (rotational speed of the matrix and potato pulp content) on the kinetic durability of the obtained granules is shown in Figure 6.



**Figure 6.** Impact of the potato pulp and rotational speed of the matrix on the kinetic durability of onion husk granules.

After analyzing Figure 6, it was found that an increase in the potato pulp content from 10% to 20% in the onion husk mixture resulted in a slight decrease in the kinetic durability of the obtained granulate at each of the tested rotational speeds of the granulator matrix. For example, increasing the content of the potato pulp from 10% to 20% in the mixture with onion husks at a matrix rotational speed of 170 rpm caused a decrease in the kinetic durability of the obtained granulate from 99.5% to 99.3%.

It should be noted that the addition of potato pulp to the onion husks allowed high-quality granules to be obtained, i.e., high kinetic durability (99.5%–98.2%). In addition, these are higher values than those obtained for onion husk granules without the use of a binder [28]. This is caused by the action of potato starch, which, in combination with moisture and high temperatures, forms a sticky gel during granulation [50]. After cooling, the gel leads to the formation of strong bonds between the particles of the mixture. As reported by Kaliyan and Morey [53], under the influence of thickening pressure, natural biomass binders may soften in the presence of moisture (e.g., water-soluble carbohydrates) or in some cases at elevated temperature (e.g., lignin, protein, starch, and fat).

After removing the pressure and cooling, the binder cures to form bridges (bonds) between the particles. As a result, the particles join together, increasing the durability of the resulting product. In addition, the activation (softening) of natural ingredients bound by moisture and temperature in the glass transition is necessary for the production of very durable briquettes and granules.

The tests (Figure 6) allowed the statement that an increase in the rotational speed of the matrix from 170 to 270 rpm caused a slight decrease in the kinetic strength of the granulate obtained from a mixture of onion husk and potato pulp (by approximately 1%), at each of the tested levels of potato pulp. For example, increasing the rotational speed of the matrix from 170 to 270 rpm with a 10% addition of potato pulp in the mixture caused a decrease in the kinetic durability of the obtained granulate from 99.5% to 98.6%.

The high degree of comminution of agglomerated particles had a favorable effect on the value of kinetic durability in the case of onion skins (Figure 6). This is confirmed by Kaliyan and Morey [54], who listed the moisture content and particle size of the compacted material as one of the most important factors that affects the magnitude of forces during the compaction process. Alakangas and Paju [55], Obidziński [56], and Hejft [57] claim that the rotational speed of the matrix influences the value of thickening pressures, while lowering the rotational speed results in higher thickening pressures, and thus granules with higher kinetic durability are obtained.

The multiple regression coefficient for the tested model (equation) was  $R^2 = 93.95\%$ , which means a good fit of the model describing the kinetic strength of the onion husk granulate depending on the addition of potato pulp and the rotational speed of the granulator matrix.

The influence of process and materials factors (rotational speed of the matrix and potato pulp content) on the density of obtained granules is shown in Figure 7.



**Figure 7.** Impact of the potato pulp and rotational speed of the matrix on the density of onion husk granules.

From Figure 7, it was found that an increase in the potato pulp content from 10% to 20% in the mixture with onion husk resulted in a decrease in the physical density of the obtained granulate from 1225.62 to 1001.36 kg·m<sup>-3</sup>, at all tested rotational granulator matrix speeds. The highest physical density (1225.62 kg·m<sup>-3</sup>) was obtained for pellets obtained from onion skins with 10% potato pulp, at a matrix speed of 170 rpm. With an increase in the amount of additive from 10% to 20%, a decrease in granulate density was observed. For example, at 170 rpm, this decrease was about 11%.

On the basis of the descriptive statistics (Figure 7), it was found that mixtures with the rotational speed of 170 rpm were characterized by the greatest variation in physical density while the lowest values were obtained at 270 rpm.

The physical density values of onion granules obtained during the tests with the addition of potato pulp were similar to the physical density of granules obtained from agglomerated onion skins without its addition [28].

It should be noted that as the amount of potato pulp added increases, the moisture content of the agglomerated mixture also increases. Moisture content, which acts as a lubricant and binder in the agglomeration process [58], is considered the most important factor affecting the quality of granules [56,57,59]. Mani and colleagues [60] claim that pellets made from maize with lower moisture

contents (5%–10%) have a higher density than those with moisture contents above 15%. This is confirmed by Shaw and Tabil [61], who, like many other researchers, stated that the lower humidity of the compacted material increases the density of the obtained granulate. Obidziński [27], by thickening buckwheat hulls with 15%, 20%, and 25% potato pulp addition, stated that the decrease in granulate density along with the increase in the pulp is caused by a decrease in the friction coefficient of the material against the walls of the holes in the granulator's matrix.

The bulk density of the obtained pellets ranged from 580 kg $\cdot$ m<sup>-3</sup> for pellets produced with the addition of 20% of potato pulp to 640 kg $\cdot$ m<sup>-3</sup> for the 10% addition.

The multiple regression coefficient for the tested model (equation) was  $R^2 = 99.62\%$ , which means a good fit of the model describing the physical density of onion husk granules depending on the addition of potato pulp and rotational speed of the granulator matrix.

The influence of the process and materials factors (rotational speed of the matrix and potato pulp content) on the demand for granulator power of the obtained granules is shown in Figure 8.



**Figure 8.** Potato pulp content and rotational speed of the matrix on the granulator demand for power during the production of granulated onion husks.

After analyzing Figure 8, it was found that along with the increase in the proportion of potato pulp from 10% to 20% in the mixture with the onion husk, the granulator demand for power decreased. For example, increasing the content of potato pulp from 10% to 20% in the mixture (at a rotational speed of 170 rpm) caused a decrease in the granulator demand for power from 3.25 to 2.23 kW. The reduction in the power demand was caused by a significant increase in moisture in the mix, which resulted from the increased content of the potato pulp. According to Obidziński and colleagues [50], Obidziński [25,27], and Obidziński and Hejft [29], increasing the content of potato pulp in the mixture results in an increase in the binder content (in the form of moisture and starch) during the granulation process. The binder reduces the resistance to the mixture being pressed through the die holes while also reducing the granulator's demand for power. The use of high moisture waste as a binder in granulation processes has also been described by Stahl and Berghel [22], who produced fuel pellets from a mixture of sawdust and post-production turnip waste resulting from the production of turnip oil. They found that as the turnip waste content in the compacted mixture increased, the energy consumption of the pelleting process decreased. Mediavilla et al. [61], by adding corn starch (in an amount of 2.5%, 5.0%,

and 7.0%) to the agglomerated mix, obtained a reduction in the power demand of the granulator while at the same time improving the process stability. Brunerová et al. [62], who produced bio-briquettes from waste biomass of tropical fruits (durian, coconut, coffee, cacao, banana, and rambutan), found that the energy demands to produce bio-briquettes from such feedstock materials were lower. The best results (lowest energy consumption in combination with high bio-briquette bulk density) were obtained from the rambutan, durian, and banana samples. Cui et al. [63] produced wood pellets and investigated the usefulness of microalgae as a binder substance to improve the physical and thermal properties of an obtained pellet, decreasing the energy consumption during their production. It was found that under appropriate conditions of pressure (120–200 MPa), temperature (80–160 °C), and moisture content (6%–14%), microalgae can effectively increase the mechanical durability and bulk density of the pellets and can notably reduce the energy consumption of the pelleting process by 23.5% to 40.4%.

The tests (Figure 8) allowed the statement that along with the increase of the rotational speed of the granulator matrix, its power demand increases. For example, an increase in the rotational speed of the matrix from 170 to 270 rpm during agglomeration of the mixture with 10% potato pulp, resulted in an increase in the power demand from 3.25 to 5.99 kW. According to Obidziński [55,64], the speed of the pelleting system most often increases the power demand of the pelletizer; however, it is also highly dependent on the specifics of the agglomerated material.

The multiple regression coefficient for the tested model (equation) was  $R^2 = 96.99\%$ , which means a good fit of the model describing the power demand of the granulator during the production of onion husk granules depending on the addition of potato pulp and the rotational speed of the granulator's matrix.

Pellets with the highest obtained kinetic durability (90% onion husk and 10% potato pulp) were used in the combustion process due to the automatic fuel dosing system, which requires high-quality pellets. They were also the granules with the highest calorific value among those produced (Figure 4).

#### 3.3. Emissions

Table 2 shows the results of the combustion of onion pellets with the addition of 10% potato pulp. There are no reports in the literature regarding emissions from the combustion of waste onion husks in low-power installations. Therefore, the results obtained were compared to granulates made from cherry stones with the addition of rye bran, which were subjected to combustion in the same installation under similar process conditions [16].

Parameter	Value		
i arameter	Onion Husks + Potato Pulp	Cherry Stones + Rye Bran [16]	
CO <sub>2</sub> [%]	7.27	7.20	
CO [mg·Nm <sup>-3</sup> ]	703.98	432.45	
$SO_2 [mg \cdot Nm^{-3}]$	216.47	38.62	
NO [mg·Nm <sup>-3</sup> ]	307.14	264.69	
HCl [mg·Nm <sup>-3</sup> ]	36.63	4.38	
The actual oxygen concentration in the exhaust [%]	14.78	10.96	
λ [-]	3.20	2.04	
Average flue gas temperature in the boiler outlet [°C]	120	170	

**Table 2.** Fluegas composition and conditions of combustion of onion husks with 10% potato pulp compared to pellet made of cherry stones with 20% rye bran.

From 1 January 2020, only boilers meeting the European Parliament Ecodesign Directive will be able to be installed in the European Union, which extends the requirements of PN EN-303-5:2012 [65] as a limit for seasonal emissions of nitrogen oxides,  $NO_x$ . The Ecodesign Directive will regulate the emission of  $NO_x$  to less than  $200 \text{mg} \cdot \text{m}^{-3}$  for combustion installations of power lower than 500 kW. Due to the negligible amounts of  $NO_2$  in the exhaust gas, only the NO content is given in Table 2 and compared in the discussion of the  $NO_x$  emission requirements. During combustion, the nitrogen

contained in the fuel is nearly completely converted into gas nitrogen,  $N_2$ , and nitrogen oxides, so-called  $NO_x$  [66]. Furthermore, the air supply, furnace geometry, combustion temperature, and combustion technology type selected are the main variables having an effect on the  $NO_x$  formation [46,67,68].

In Table 2, the actual average quantity of oxygen in the flue gas is given based on the calculated air excess ratio,  $\lambda$ . The difference in the coefficient,  $\lambda$ , for pellets from onion husks and cherry stones is clearly visible. In accordance with Pudlik [69], the air excess ratio,  $\lambda$ , depends on the fuel type and the device in which it is combusted. In terms of waste combustion, it can reach values of 2 to 2.5. However, the higher the  $\lambda$ , the worse the contact conditions of air with the flammable particles.

Obernberger [70] claims that problems related to  $SO_x$  emissions can be expected when the sulfur content in biomass exceeds 0.2% by weight, which was reached for both tested wastes: Onion husks and potato pulp. The importance of sulfur is not mainly due to  $SO_x$  emissions but to its role in corrosive processes. According to Spiegel [71] and Obernberger [72], high  $SO_x$  concentrations in exhaust gas contribute to the sulfurization of alkali metal chlorides by reducing the exhaust gas temperature, which leads to the release of chlorine. If these reactions occur in ash particles precipitated on the surface of the heat exchanger tubes, the chlorine released can cause corrosion by forming FeCl<sub>2</sub> or ZnCl<sub>2</sub> on the heat exchanger surfaces. The presence of sulfur in fuels has a certain positive effect, i.e., a reduction in the risk of chloride corrosion due to the change of the chloride ion in sodium or potassium chlorides to the sulfate ion, which is more temperature stable than chloride [72,73]. Hardy and colleagues [74] report that the risk of chloride corrosion does not occur if the content of chlorine in biomass does not exceed 0.02%. Exceeding this limit was observed only in the case of onion husk. The calculated S/Cl ratio for onion husk is about 19.7; therefore, it is much higher than 2.2, and according to literature data [74], the risk of high temperature chloride corrosion is very low. The same authors, Hardy and co-workers [74], claim that counteracting the effects of chloride corrosion can be also based on an assessment of the corrosion threat for a given biomass using the fuel corrosion indicator, where the ratio of sulfur to chlorine in fuel and the share of potassium are taken into account. In this case, further analysis must be provided to investigate the usefulness of onion husk in combustion processes. Onion husk, when used as the main fuel component, contributes to the increase of  $SO_2$  emissions; however, as an addition to raw materials rich in chlorine, it may positively reduce the risk of chloride corrosion. Chlorine contained in biomass is mostly released in the form of hydrogen chloride, HCl, during combustion [75], which can later react with other flue gas components and lead to the production of dioxins [76]. The content of HCl in the exhaust from onion husk pellet combustion is approximately nine times higher than that from the combustion of cherry stones pellets. Rabacal et al. [77] state that the type of granulate significantly affects the boiler efficiency and emission characteristics.

In combustion processes, specific attention is paid to the content of CO in flue gas as a symptom of the presence of soot, hydrocarbons, dioxins, and furans [78]. The maximum CO content in exhaust from boilers with a heating capacity lower than 0.5 MW is regulated by the Ecodesign Directive and cannot exceed 500 mg·m<sup>-3</sup> (when the biomass fuel feeding is automatic), which was also a state of PN EN-303-5: 2012 for five class boilers [65]. The high CO emission value obtained during the combustion of onion husk granules with the addition of potato pulp indicates problems in the oxidation of CO to  $CO_2$  and the low stability of the combustion process [79–82]. Sornek and co-workers [83], in controlling the operation of a stove with the use of a PLC controller (enabling the control of the amount of air dispensed to the combustion chamber) and an exhaust gas analyzer (taking into account mainly CO emissions), state that it is possible to achieve the operating parameters required by the BImSchV 2 and Ecodesign standards.

# 4. Conclusions

The densification process (pressure agglomeration, granulation), its energy consumption, efficiency, and the quality of the obtained product are related to many material, apparatus, and process factors. The deciding objective of the creation of fuel pellets from agri-food waste is the need to develop

new management systems of production residues, which will allow a reduction of the costs of their utilization due to their use in energy production systems.

The pressure agglomeration process of wastes from the agri-food industry requires the selection of appropriate material, process, and equipment conditions for each type of waste. The highest quality of pellets from onion skins and potato pulp was obtained with the 10% potato pulp addition and the rotational speed of the granulator matrix as  $n_m = 170$  rpm.

The use of potato pulp as a binder reduces the calorific value and heat of combustion of the granulate; however, due to the content of starch and its binding properties, at the granulation temperature, it facilitates the process, acting as a lubricant and reduces the granulator's demand for power.

The conducted tests of the combustion of the produced granules allowed verification of their usefulness as solid fuels for use in low-power boilers with a retort grate. Due to the high content of CO and NO, which do not meet the requirements of the Ecodesign Directive and high SO<sub>2</sub> emission, further research must be carried out in the case of thermal utilization of onion husks for energy purposes. The authors suggest that due to the high sulfur content, it is possible to add onion husks to materials with high chlorine contents, which could result in a lower risk of chloride corrosion. Optimized boiler structures for biomass combustion, equipped with systems for mixing secondary air with combustion products, can lead to a reduction in NO<sub>x</sub> and CO emissions and allow the combustion of fuels formed from agri-food waste, whose thermal processing is difficult in installations with a less complicated structure.

The research carried out on the pressure agglomeration of agri-food waste and its thermal utilization allows the statement that there is a need to carry out comprehensive analyses on the granulation of plant waste materials available on the Polish market, which will allow the selection of the best composition of agglomerates in terms of their subsequent use as fuel for combustion, with the possibly limited emission of compounds harmful to the environment and human health. Moreover, considerations on the use of agri-food waste in energy systems require a deeper analysis of their usefulness, e.g., analysis of the composition of the soot formed, analysis of the dust content in exhaust gases, and examination of the content of long-chain compounds in exhaust gases. This work is an introduction to these considerations and requires further analysis.

Author Contributions: For research articles with several authors, a short paragraph specifying their individual contributions must be provided. The following statements should be used "conceptualization, M.D. and S.O.; methodology, S.O.; software, M.K.-S.; validation, M.D., M.K.-S. and S.O.; formal analysis, M.D.; investigation, M.D.; resources, K.J., M.D., S.O., P.S.; data curation, M.D., M.K.-S., K.J. and S.O.; writing—original draft preparation, M.D.; writing—review and editing, M.D., P.S. and S.O.; visualization, M.K.-S.and S.O.; supervision, S.O.; project administration, S.O.; funding acquisition, S.O."

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