



Article

Thermal Performance for Wet Cooling Tower with Different Layout Patterns of Fillings under Typical Crosswind Conditions

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Abstract: A thermal-state model experimental study was performed in lab to investigate the thermal performance of a wet cooling tower with different kinds of filling layout patterns under windless and 0.4 m/s crosswind conditions. In this paper, the contrast analysis was focused on comparing a uniform layout pattern and one kind of optimal non-uniform layout pattern when the environmental crosswind speed is 0 m/s and 0.4 m/s. The experimental results proved that under windless conditions, the heat transfer coefficient and total heat rejection of circulating water for the optimal non-uniform layout pattern can enhance by approximately 40% and 28%, respectively, compared with the uniform layout pattern. It was also discovered that the optimal non-uniform pattern can dramatically relieve the influence of crosswind on the thermal performance of the tower when the crosswind speed is equal to 0.4 m/s. For the uniform layout pattern, the heat transfer coefficient under 0.4 m/s crosswind conditions decreased by 9.5% compared with the windless conditions, while that value lowered only by 2.0% for the optimal non-uniform layout pattern. It has been demonstrated that the optimal non-uniform layout pattern has the better thermal performance under 0.4 m/s crosswind condition.

Keywords: wet cooling tower; non-uniform layout filling; thermal performance; crosswind

1. Introduction

Cooling towers are widely used to extract heat from warm water to the atmosphere in most power stations, refrigeration, and air conditioning industries [1,2]. They can be classified by means of contacting mode into dry [3,4] and wet types. Moreover, they can also be classified by the driving force of air stream as mechanical-draft [5,6] and natural-draft types. As one of the main types, the natural-draft wet cooling towers play an important role to cool the circulating water from the condenser in thermal power plants or some inland nuclear power plants, and the cooling towers can directly affect the total power generation capacity [7]. Based on prior studies, 70% of heat extraction capacity occurs in the filling zone [8]. Therefore, it is extremely necessary to study the thermal performance of the filling zone.

Many researchers have focused on the thermal performance of fillings for wet cooling towers, and early research traces back to the 1940s [9–11]. Briefly, the research regarding fillings can be divided into three aspects, which are theoretical mathematical model research [12–15], lab-based model experiments [16–19], and numerical computation [20–23].

However, the prior studies failed to discuss the height difference of the filling layout, and regarded fillings as the same height in different radii inside the tower. Actually, a uniform layout fillings pattern is obviously unreasonable due to the non-uniform air dynamic field inside the tower. Thus, studies

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regarding the layout pattern of fillings are extremely crucial to further energy-saving research for wet cooling towers. Gao et al. [24] performed a thermal-state model experiment to investigate the influence of filling layout pattern on thermal performance of a wet cooling tower, including the cooling temperature difference, cooling efficiency, Merkel number, Lewis number, and ratio of evaporative heat rejection, and obtained one kind of optimal non-uniform pattern. However, Gao et al. did not research the change rules of heat transfer coefficient and total heat rejection of circulating water—which are extremely significant for analysis of the thermal performance of wet cooling towers—and furthermore, their study did not consider crosswind conditions.

Consequently, in this paper, studies of filling layout patterns inside wet cooling towers are conducted via a basic thermal-state model experiment to reveal the change rules of heat transfer coefficient and total heat rejection of circulating water under windless and typical crosswind conditions, with the further aim of determining the influence of filling layout patterns on the thermal performance of wet cooling towers under a typical crosswind speed value of 0.4 m/s.

2. Experimental Study Design

2.1. Experimental Setup and Operating Conditions

The experimental setup is displayed via the schematic diagram depicted in Figure 1.

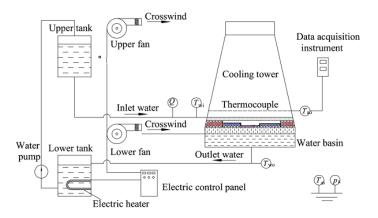


Figure 1. Schematic diagram of the experimental cooling tower.

The model tower adopted in this experiment is designed to simulate a typical wet cooling tower in large-scale power plants in terms of the geometry similarity, Froude number similarity, and wind velocity scale similarity, which are detailed in [25–28]. Additionally, the relevant scale measure of model to prototype tower is 1:100, and the details of the primary measurement setup and instruments are listed in Table 1.

Items	Measuring Instruments	Accuracy	
Atmospheric pressure	Hot-wire manometer (KA31)	±3%	
Inlet dry and wet bulb temperature	Psychrometer	±0.1 °C	
Outlet air temperature	Copper-constantan thermocouple	±0.3 °C	
Inlet and outlet water temperature	Mercury thermometer	±0.1 °C	
Air humidity	Hygrometer (HI8564)	$\pm 2\%$	
Circulating water flow rate	Rotameter	$\pm 1.5\%$	

Table 1. Monitored parameters and measurement instruments.

During the whole experiment, the circulating water inlet temperatures were 50 $^{\circ}$ C, 55 $^{\circ}$ C, and 60 $^{\circ}$ C. The circulating water rates were 4 L/min, 6 L/min, and 8 L/min, and the crosswind speed

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was chosen to be 0.4 m/s, which was monitored by the lower fan marked in Figure 1. Additionally, five types of filling layout patterns [24] used in this study are detailed in Section 2.2.

2.2. The Determination of Typical Crosswind Speed

According to the research works [25–28] from Group Gao, the performance parameters of wet cooling towers—such as cooling efficiency, cooling temperature difference, Merkel number, Lewis number, heat transfer coefficient, etc.—showed a shifting point when the experimental crosswind speed reached 0.4 m/s, indicating that this wind speed is a special crosswind working condition. Therefore, in this paper, the typical crosswind speed was chosen to be 0.4 m/s during the experiment, and the corresponding actual field crosswind speed was 4 m/s based on the similarity criterion.

2.3. Filling Layout Patterns inside the Model Tower

In this experiment, five kinds of layout patterns were chosen to study the change rules of two performance parameters for a wet cooling tower: heat transfer coefficient and total heat rejection of circulating water. The block plan is shown in Figure 2, and the details of different layout patterns are pointed out in detail in Table 2, where P1–P5 represent five pattern types. Additionally, the water is uniformly distributed using nozzle spray, the same distribution system in use in natural draft wet cooling towers.

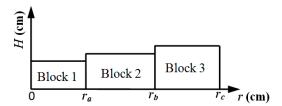


Figure 2. Block plan for non-uniform layout fillings.

Item	P1	P2	Р3	P4	P5	
	Uniform Layout Pattern	Non-Uniform Layout Patterns				
r_a (cm)	29.5	9	11	13	15	
r_b (cm)	29.5	24.7	23.2	21	19	
r_c (cm)	29.5	29.5	29.5	29.5	29.5	
r_a/r_c	-	0.31	0.37	0.44	0.51	
r_b/r_c	-	0.84	0.79	0.71	0.64	
H1 (cm)	8	4	4	4	4	
H2 (cm)	8	8	8	8	8	
H3 (cm)	8	10	10	10	10	

Table 2. Details for five different layout patterns.

P1: uniform layout pattern; P2–P5: non-uniform layout patterns.

2.4. Experimental Object

Based on the cooling temperature difference, cooling efficiency, Merkel number, Lewis number, and ratio of evaporative heat rejection, Gao et al. [24] obtained the optimal non-uniform layout pattern for which the radius ratio of r_a/r_c is approximately 0.44 and r_b/r_c is around 0.71 (refer to Figure 2 and Table 2). Higher heat transfer coefficient and total heat rejection indicate stronger cooling performance. Thus, this study focused mainly on the change rules of the heat transfer coefficient and total heat rejection of circulating water under the different layout patterns, and on analyzing the effect of optimal non-uniform fillings on these two parameters under windless and 0.4 m/s crosswind conditions.

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3. Experimental Results and Analysis

3.1. Influence of Filling Layout Patterns on Performance Parameters under Windless Conditions

Under the windless conditions, the relationship curves between heat transfer coefficient, total heat rejection of circulating water, and five kinds of layout patterns are shown in Figures 3 and 4 for two different operating conditions, with the circulating water inlet temperature being 50 $^{\circ}$ C and 60 $^{\circ}$ C, and the circulating water rate being 6 L/min.

In this thermal-state model study, drift losses are slight and can be neglected, so the heat transfer coefficient α_v is defined by

$$\alpha_v = \frac{C_{ma} \cdot G(\theta_2 - \theta_1)}{(t_m - \theta_m) \cdot V} \tag{1}$$

In the formula above, C_{ma} is the specific heat of wet air at the outlet of the model tower (kJ/kg °C); G is the airflow rate (kg/s); and θ_1 and θ_2 represent the inlet and outlet air temperature of the model tower (°C). Additionally, t_m is the average value of inlet and outlet circulating water temperature, and θ_m is the average value of θ_1 and θ_2 . Finally, V represents the exit area of fillings (m²).

Figure 3 describes the change rules of heat transfer coefficient under five kinds of layout patterns. The heat transfer coefficient under non-uniform fillings is obviously higher than that under the uniform pattern, and pattern P4 is the optimal non-uniform layout pattern. Experimental results demonstrate that—compared with the uniform layout pattern (P1)—the heat transfer coefficient in P4 pattern can increase by approximately 40%.

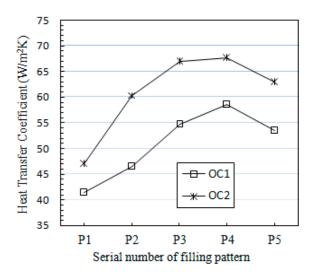


Figure 3. Relationship curves between heat transfer coefficient and filling layout patterns. OC1: Operating conditions 1 (50 °C, 6 L/min); OC2: Operating conditions 2 (60 °C, 6 L/min).

Figure 4 explains the change rules for total heat rejection of circulating water under five kinds of layout patterns. Almost the same rules as for heat transfer coefficient can be drawn from Figure 4. This is because a larger total heat rejection indicates a stronger cooling performance. Obviously, the thermal performance is excellent under non-uniform patterns in terms of the total heat rejection of circulating water—especially with pattern P4. Additionally, the relative increase of the total heat rejection under pattern P4 was around 28%, compared with the uniform pattern P1.

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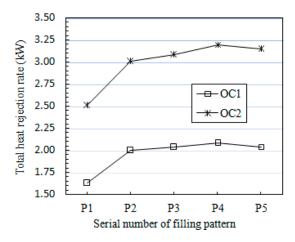


Figure 4. Relationship curves between total heat rejection and filling layout patterns. OC1: Operating conditions 1 (50 °C, 6 L/min); OC2: Operating conditions 2 (60 °C, 6 L/min).

Apparently, according to the heat transfer coefficient and total heat rejection of circulating water, the thermal performance of wet cooling towers under non-uniform fillings can be much higher than that of uniform filling patterns. Meanwhile, this study pointed out that under windless conditions, the heat transfer coefficient and total heat rejection of circulating water for the optimal non-uniform pattern (pattern P4) can enhance about by 40% and 28%, respectively, compared with the uniform pattern.

3.2. Influence of Filling Layout Patterns on Performance Parameters under 0.4 m/s Crosswind Conditions

The experimental study by Gao et al. [25,26] proved that the thermal performance of wet cooling towers dropped dramatically under 0.4 m/s crosswind speed conditions. To this end, the current study limits the crosswind speed at 0.4 m/s to investigate the thermal performance of the tower under a non-uniform pattern.

Under windless and 0.4 m/s crosswind speed conditions, the relationship curves between heat transfer coefficient, total heat rejection of circulating water, and five layout patterns are shown in Figures 5 and 6, with the circulating water inlet temperature being 60 $^{\circ}$ C and the circulating water rate being 6 L/min.

It can be seen in Figure 5 that, for five layout patterns, the heat transfer coefficient under 0.4 m/s crosswind speed drops strongly compared with windless conditions.

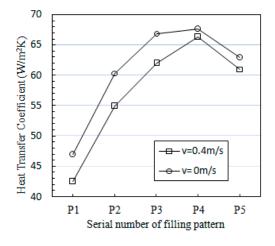


Figure 5. Relationship curves between heat transfer coefficient and filling layout patterns under 0.4 m/s crosswind speed conditions. Operating conditions: $60 \,^{\circ}\text{C}$, $6 \,^{\circ}\text{L/min}$.

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Experimental study shows that, for uniform pattern P1, the heat transfer coefficient under 0.4 m/s crosswind conditions decreased by 9.5% compared with that of the windless condition. For pattern P4, the heat transfer coefficient under 0.4 m/s crosswind condition decreased by only 2.0% compared with the windless condition. Almost the same rules can be observed for total heat rejection in Figure 6. For pattern P1, the total heat rejection under 0.4 m/s condition decreased by approximately 7% compared with the windless condition; for pattern P4, however, that value under 0.4 m/s condition drops by only 3.5% compared with the windless condition.

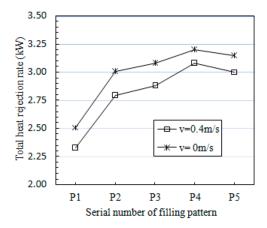


Figure 6. Relationship curves between total heat rejection and filling layout patterns under 0.4 m/s crosswind speed conditions. Operating conditions: 60 °C, 6 L/min.

The air temperature and humidity near the tower center are higher than those outside the tower. Therefore, the driving force near the tower center would decrease, and the air dynamic field inside the tower is also non-uniform, in turn leading to a smaller wind speed through the fillings near the tower center. At the same time, the wet air near the tower center is close to saturated, and the heat and humidity absorption potential of air near the tower center becomes relatively weak. Consequently, the fillings near the tower center should be thinner. In this study, according to the analysis of the heat transfer coefficient and total heat rejection of circulating water, it can be said that the optimal non-uniform pattern (i.e., P4, for which the radius ratio of r_a/r_c is approximately 0.44 and r_b/r_c is around 0.71) can relieve the influence of crosswind on the tower's thermal performance when the crosswind speed is equal to 0.4 m/s. The main reason for this is that pattern P4 has a smaller airflow resistance in the center zone of the tower according to the above analysis, which can draw cold air into the tower.

4. Conclusions

- (1) Under windless conditions, the heat transfer coefficient and total heat rejection of the circulating water for the optimal non-uniform layout pattern increases by 40% and 28%, respectively, compared with the uniform pattern.
- (2) Based on two performance parameters (heat transfer coefficient and total heat rejection of circulating water), the optimal non-uniform pattern—with the radius ratio $r_a/r_c \sim 0.44$ and $r_b/r_c \sim 0.71$ can dramatically relieve the influence of crosswind on the thermal performance of wet cooling towers when the crosswind speed is equal to 0.4 m/s.
- (3) Compared with the windless condition, the heat transfer coefficient under 0.4 m/s condition decreased by 9.5% for the uniform layout pattern, while that value under 0.4 m/s condition decreased by only 2.0% for the optimal non-uniform layout pattern.

Currently, we are analyzing the change rules of some typical performance parameters (including cooling efficiency, cooling temperature difference, Merkel number, heat transfer coefficient, etc.) under

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different crosswind conditions (including 0.1 m/s, 0.2 m/s, 0.3 m/s, 0.5 m/s, 0.6 m/s, 0.7 m/s, and 0.8 m/s) when adopting non-uniform layout fillings. We will also try to use the field synergy theory to analyze and reveal the advantage of non-uniform fillings based on the experimental data.

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Author Contributions: Ming Gao designed the experiment system, conducted the model experiment and wrote the manuscript, Chang Guo and Chaoqun Ma compiled the literatures and collected the experimental data together. Yuetao Shi analyzed the experimental data. Fengzhong Sun checked and revised the whole manuscript.

Conflicts of Interest: The authors declare no conflict of interest.

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