



Article

Removal Efficiency and Risk Assessment of Polycyclic Aromatic Hydrocarbons in a Typical Municipal Wastewater Treatment Facility in Guangzhou, China

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Abstract: The loading and removal efficiency of 16 US EPA polycyclic aromatic hydrocarbons (PAHs) were examined in an inverted A²/O wastewater treatment plant (WWTP) located in an urban area in China. The total PAH concentrations were 554.3 to 723.2 ng/L in the influent and 189.6 to 262.7 ng/L in the effluent. The removal efficiencies of Σ PAHs in the dissolved phase ranged from 63 to 69%, with the highest observed in naphthalene (80% removal). Concentration and distribution of PAHs revealed that the higher molecular weight PAHs became more concentrated with treatment in both the dissolved phase and the dewatered sludge. The sharpest reduction was observed during the pretreatment and the biological phase. Noncarcinogenic risk, carcinogenic risk, and total health risk of PAHs found in the effluent and sewage sludge were also assessed. The effluent BaP toxic equivalent quantities (TEQ_{BaP}) were above, or far above, standards in countries. The potential toxicities of PAHs in sewage effluent were approximately 10 to 15 times higher than the acceptable risk level in China. The health risk associated with the sewage sludge also exceeded international recommended levels and was mainly contributed from seven carcinogenic PAHs. Given that WWTP effluent is a major PAH contributor to surface water bodies in China and better reduction efficiencies are achievable, the present study highlights the possibility of utilizing WWTPs for restoring water quality in riverine and coastal regions heavily impacted by PAHs contamination.

Keywords: polycyclic aromatic hydrocarbons; municipal effluents; risk assessment; wastewater treatment; sludge; inverted A^2/O process

1. Introduction

Polycyclic Aromatic Hydrocarbons (PAHs) are a wide spread class of environmental pollutants of concern [1] due to their carcinogenicity, mutability and toxicity [2]. They originate primarily from incomplete combustion and petroleum spill [3] and are prone to bioaccumulation and biomagnification [4] as well as long-distance transport [5]. Due to their toxicity, PAHs have been listed as contaminants that required monitoring. 16 PAHs have been enlisted for priority monitoring by US EPA and 7 PAHs selected as target PAHs by China National Environmental Monitoring Center [6]. Further, PAH concentration limits have been set by many countries, such as EU [7], US EPA [8], Netherlands [9] and China [10].

Following their release from fuel spillage or atmospheric deposition, PAHs can enter the sewage system through domestic wastewater, industrial discharge, or surface runoff via the urban drainage. In WWTP, PAHs may exist in the dissolved phase or in the sorbed form, attached to sludge or organic-rich suspended solids. The partitioning behavior of PAHs is well understood [11], it is expected that the low molecular weight (LMW) PAHs are mainly in dissolved form whereas the high molecular weight (HMW) PAHs are predominantly bound to organic-rich surfaces or solids.

In China, the growing attention on the pollution of water bodies has led to increasingly stringent sewage discharge standards [12]. WWTPs with conventional treatment process were hard pressed to meet this task with efficiency and economy [13]. The Anaeroic-Anoxic-Aerobic (A^2/O) treatment process has been widely adopted to address the extensive problem of eutrophication in both freshwater bodies and coastal areas. A^2/O generally exhibits better performance in nitrogen and phosphorus removal than other treatment processes, probably benefiting from the lower extracellular polymeric substances production in A^2/O sludge [14]. Given the growing number of A^2/O treatment facilities in China [13,15], it is important to investigate the fate of PAHs through the A^2/O process for improving their removal in both existing and new WWTPs.

The aims of the present study were to (1) investigate the loading and removal of dissolved PAHs in a WWTP with inverted A^2/O process; (2) characterize the profiles of PAHs at different stages of the WWTP; and (3) assess the health risks of PAHs associated with the effluent and the sludge.

2. Materials and Methods

2.1. Chemicals

A PAH standard solution mix was purchased from o2si Smart Solutions (Charleston, SC, USA). The mix included naphthalene (NAP), acenaphthylene (ANE), acenaphthene (ANA), fluorene (FLU), phenanthrene (PHE), anthracene (ANT), fluoranthene (FLT), pyrene (PYR), benzo(a)anthracene (BaA), chrysene (CHR), benzo(b)fluoranthene (BbF), benzo(k)fluoranthene (BkF), benzo(a)pyrene (BaP), indeno(1,2,3-cd)pyrene (IcdP), dibenzo(a,h)anthracene (DBA) and benzo(g,h,i)perylene (BghiP).

2.2. Wastewater Treatment Plant

The studied WWTP was located in Guangzhou, China. It collected combined sewage in canal from the districts of Liwan and Yuexiu and part of the Baiyun district. The core biological treatment was the anoxic-anaerobic-aerobic (Inverted A^2/O) process which helped to achieve better nitrogen and phosphorus removal. The WWTP had a design treatment capacity of 2.2×10^5 m³/d. All tanks and units in the WWTP, except the secondary clarifier, were closed from the atmosphere and have been installed with deodorization devices and ventilation systems.

2.3. Sampling

Wastewater samples were collected from 6 sampling points (Figure 1) including the influent (IN), the effluent of grit chamber (EG), the water-sludge mixture in aerobic stage (AS), the effluent of inverted A^2/O tank (EA), the effluent of the secondary clarifier (ES) and the final effluent after chlorination (FE). At each sampling point, 8 grab samples were collected evenly every 3 h to produce

an 8-L 24-h composite sample. All collected aqueous samples were stored in amber glass bottle and were filtered immediately. Dewatered sludge samples (DS) were collected from sludge dewatering house and stored at $-20\,^{\circ}$ C in lab. Sampling campaigns were conducted on 4 rain-free weekdays between late November and December 2015.

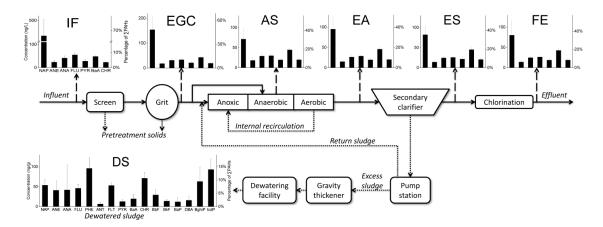


Figure 1. Treatment stages in the WWTP and the sampling points for PAHs. Error bars represent 1 standard deviation of the mean. IN = influent; EG = the effluent of grit chamber; AS = the water-sludge mixture in aerobic stage; EA = the effluent of inverted A^2/O tank; ES = the effluent of the secondary clarifier; FE = the final effluent after chlorination; DS = dewatered sludge.

2.4. Chemical Analyses

The wastewater samples were filtrated with 0.7 μ m glass fiber filters (Whatman, GF/F) by disc filters. Before use, glass fiber filters were baked at 450 °C in muffle furnace for 5 h to remove trace organic carbon. The filtrated samples (500 mL) were processed by solid-phase extraction (SPE) using an automated extractor (AQUA Trace ASPE799, GL Sciences, Inc., Tokyo, Japan). The SPE stationary phases were conditioned with sequential elution of dichloromethane (5 mL), ethyl acetate (5 mL), methanol (10 mL) and Milli-Q water (10 mL). The samples were passed through the cartridges at a flow rate of 10 mL/min. The cartridges were dried under high purity nitrogen. The analytes were subsequently eluted by ethyl acetate (3 mL) and dichloromethane (3 mL). The combined extracts were evaporated by nitrogen to nearly dry and diluted to 1 mL with ethyl acetate in brown glass vials at 4 °C until chemical analyses. Chemicals used above were all of chromatography grade. The dewatered sludge samples were freeze-dried, ground into powder and passed through 0.2 mm sieve. Sludge PAHs were extracted following the procedure reported in Wu et al. [16].

Sample PAHs concentrations were analyzed in selective ion monitoring mode using Agilent 7890A/5975C (GC-MS, Agilent Technologies, Inc., Palo Alto, CA, USA) equipped with Agilent DB-5MS column (30 m \times 0.25 mm (i.d.) with 0.25 µm film thickness, Agilent, Santa Clara, CA, USA). The column temperature program was as follows: temperature increased to 60 °C (1-min hold), 110 °C at 15 °C/min (1-min hold), then successively to 180 °C at 20 °C/min, 203 °C at a rate of 2 °C/min, and 250 °C at a rate of 5 °C/min, and finally to reach 310 °C at 2 °C/min. Pure helium was used as the carrier gas at a flow rate of 1.3 mL/min. 1 µL sample was injected into the injector with an initial temperature of 300 °C using splitless injection mode. The mass spectra were obtained using electron ionization mode at 70 eV and 250 °C.

2.5. Quality Assurance and Quality Control

Procedural blanks, spiked blanks (standards spiked into solvent), sample replicates (n = 3) and matrix spikes were used to monitor the extraction and analytical quality for the samples. Recoveries of all the PAHs except NAP fell within the range of 65.9 to 111.3%. Recoveries of NAP fell within the range of 38.1 to 51.3%. The relative standard deviations in all replicates were less than 15% as

recommended by the US EPA Method 8270D [17]. Instrument detection limits for all individual PAHs were defined as three times of the signal-to-noise ratio.

2.6. Toxicity Assessment

2.6.1. Toxic Equivalent Quantity

The combined toxicity of different PAHs in wastewater and sludge samples was evaluated using the BaP toxic equivalent quantity (TEQ_{BaP}) [18]. This widely applied method [19–21] calculates TEQ_{BaP} using the aqueous phase concentration for the *i*th PAH, C_i , and the prescribed toxic equivalent factors (TEFs) (Table 2; [18]) from the following equation [22]:

$$TEQ_{BaP} = \sum (C_i \times TEF_i)$$
 (1)

2.6.2. Health Risk

Health risk of PAHs in aqueous samples were assessed following the US EPA health risk assessment guidelines [23] supposing the effluent as source of drinking water for downstream communities. Sixteen PAHs were divided into noncarcinogenic and carcinogenic PAHs for evaluation. Relevant parameters and PAH's classification are listed in guidance for public health risk assessment [24] and Krishnan et al. [25]. Health risk associated with the carcinogenic PAHs (i.e., BaA, CHR, BbF, BkF, BaP, DBA, and IcdP) was evaluated using Equations (2)–(4) [26,27]:

$$R_i < 0.01, R_i = D_i \times Q_i / 70$$
 (2)

$$R_i \ge 0.01, R_i = [1 - \exp(-D_i Q_i)]/70$$
 (3)

where R_i is annual carcinogenic risk for an individual PAH; D_i is daily intake for carcinogenic PAH (mg/(kg·d)); Q_i is carcinogenic intensity factor; 70 is human average lifetime (a); C_i is concentration of PAH.

$$D_i = 2.2C_i/70 (4)$$

where 2.2 is estimated water ingestion rate for adult (L/d); 70 is average weight of adult (kg).

Health risk contributed from the noncarcinogenic PAHs (i.e., NAP, ANE, ANA, FLU, PHE, ANT, FLT, PYR, and BghiP) was assessed as [26,27]:

$$R_i = (D_i \times 10^{-6} / RfD_i) / 70 \tag{5}$$

where 70 is average lifetime; RfD_i is drinking reference dose of noncarcinogen (mg/(kg·d)).

The total health risk, *R*, was determined as the sum of individual PAHs risks [26,27]:

$$R = \sum_{i=1}^{k} R_i \tag{6}$$

3. Results

3.1. PAHs in Dissolved Phase

3.1.1. Comparison between Different Dates

PAHs concentrations (Table 1) in raw sewage are generally consistent throughout the study, as the level differences across the four sampling dates are small. The influent total PAHs concentration increased by approximately 20% during the first three sampling dates but stabilized by the fourth date. The slight change in influent total PAHs level coincided with transition from autumn to winter in Guangzhou. Similar change in PAHs level has also been reported Qiao et al. [28] and was probably

associated with the increase in coal/gas burning for winter heating [29]. The relative distributions of PAHs at various treatment stages also showed little difference over sampling dates (Figure 2).

Date	Stage	2-Rings 3-Rings					4-Rings			∑HMW	ΣPAHs
Dute	Juge	NAP	ANE	ANA	FLU	PYR	BaA	CHR	PAHs	PAHs	
	IN	335.66	21.06	50.82	56.49	19.14	48.06	23.13	464.03	90.33	554.36
	EG	85.15	19.78	38.33	36.13	16.14	46.17	20.87	179.39	83.18	262.57
22.37	AS	55.91	29.16	39.83	35.95	15.36	47.90	23.70	160.85	86.96	247.81
23 November	EA	86.19	18.41	30.51	26.41	14.95	49.47	22.44	161.52	86.86	248.38
	ES	100.19	15.25	29.27	25.03	15.54	51.04	25.04	169.74	91.63	261.37
	FE	43.51	11.13	28.07	22.37	14.73	49.18	23.44	105.08	87.35	192.44
	IN	449.82	16.64	28.88	43.49	22.43	47.45	22.05	538.84	91.93	630.77
	EG	142.31	16.16	24.46	28.46	21.53	41.39	21.27	211.39	84.19	295.58
2 D	AS	103.53	14.86	24.19	27.51	22.37	44.11	18.42	170.09	84.90	254.99
2 December	EA	108.20	14.04	22.62	29.25	19.62	46.94	21.04	174.11	87.60	261.70
	ES	84.94	13.97	20.88	25.70	29.07	42.15	18.21	145.50	89.44	234.93
	FE	55.66	13.69	20.83	25.34	16.24	39.18	18.70	115.52	74.12	189.64
	IN	480.58	27.31	41.74	59.41	36.59	51.87	25.75	609.04	114.21	723.24
	EG	217.03	18.90	31.12	37.77	24.83	43.08	18.33	304.81	86.24	391.05
0 D	AS	73.94	14.53	26.56	28.68	21.56	45.19	21.04	143.70	87.79	231.49
9 December	EA	58.82	13.36	22.95	27.69	21.83	45.34	20.14	122.81	87.32	210.13
	ES	51.19	12.87	21.71	23.77	21.04	46.37	22.07	109.55	89.49	199.04
	FE	107.75	17.02	25.19	28.54	24.24	42.54	17.46	178.49	84.23	262.73
	IN	475.85	29.38	43.63	60.99	33.21	45.57	20.71	609.85	99.48	709.33
	EG	171.78	16.11	29.97	30.73	20.77	40.36	15.81	248.59	76.94	325.53
17 December	AS	51.55	13.77	24.80	26.77	18.63	40.18	15.95	116.90	74.76	191.66
17 December	EA	126.31	13.49	28.28	30.83	20.97	40.54	15.76	198.91	77.27	276.18
	ES	92.23	13.40	25.07	27.36	20.14	40.02	15.64	158.07	75.81	233.88

Table 1. Concentration of PAHs at various stages of sewage treatment (ng/L).

IN = influent; EG = the effluent of grit chamber; AS = the water-sludge mixture in aerobic stage; EA = the effluent of inverted A^2/O tank; ES = the effluent of the secondary clarifier; FE = the final effluent after chlorination; DS = dewatered sludge.

19.21

39.42

15.43

180.62

74.06

254.67

28.86

13.58

113.67

24.51

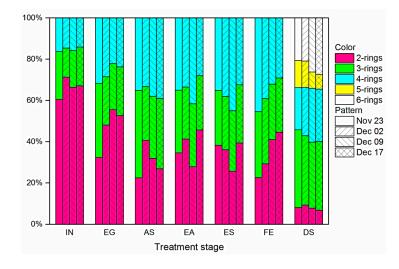


Figure 2. Distribution profiles of PAHs at the different treatment stages.

3.1.2. Concentrations of PAHs

The concentrations of dissolved PAHs at various sampling points are summarized in Table 1 and visualized in Figure 1. Only seven of the targeted PAHs were detected in the aqueous samples; the remaining PAHs were not detected, most likely due to volatilization for the LMW PAHs (i.e., \leq 3 rings) and strong sorption for the HMW species (i.e., 4–6 rings). The most abundant PAHs in the influent (IN) was naphthalene (335.66–480.58 ng/L), which accounted for more than 60% of Σ PAHs (554.36–723.24 ng/L). The high levels of IN naphthalene may be attributed to its use as precursor the

production of phthalic anhydride, a key starting material for various industrial production [30]. In the effluent samples (FE), Σ PAHs ranged from 189.64 to 262.73 ng/L with naphthalene, again, as the highest component accounting for 22 to 44%. The PAH levels observed here are comparable with those reported for another WWTP at the north of Guangzhou (Σ PAHs = 1150 ng/L) [31] but significantly higher than that measured at a Hiroshima WWTP (Σ PAHs = 60 ng/L) [32].

3.1.3. Removal Efficiencies of PAHs

The overall removal efficiencies of ∑PAHs in the dissolved phase through the WWTP was 63 to 69%. The most substantial reduction was observed on naphthalene (2-rings; 60–87%), followed by 3-rings (32–52%) and 4-rings PAHs (3–26%) (Figure 3). The observed overall removal in dissolved phase is comparable to those reported in earlier studies. Ozaki et al. [32] observed a 60% PAHs removal in a Hiroshima WWTP; Bergqvist et al. [33] reported a 30 to 60% removal in a Lithuanian sewer facility. Removal efficiencies as high as 90 to 100% have been observed in specific treatment facilities [33,34] though such performance levels is not common.

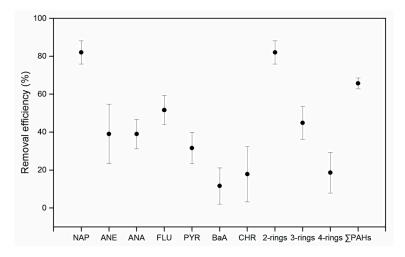


Figure 3. The removal efficiencies of PAHs in the dissolved phase. Error bars represent 1 standard deviation of the mean.

PAH concentrations generally declined along the treatment process (Figure 4). The most significant reduction in PAHs was found during the primary treatment phase (IN-EG) which included fine screen and a grit chamber-clarifier. 50 to 61% of the 2 to 3 ringed PAHs and approximately 46 to 54% of Σ PAHs were removed in this phase. The hydrophobic nature of PAHs, as indicated by their high $K_{\rm ow}$, implied that they were more likely to (ad)sorb onto solids rather than remained dissolved [35]. It is generally believed that sorption to particulate and dissolved organic matter, rather than biodegradation, is the major removal mechanism for PAHs during the primary treatment phase [36,37].

During the biological treatment stage (EG-EA), pretreated wastewater was mixed fully with returned sludge and then experiences the anoxic-anaerobic-aerobic (Inverted A^2/O) process. Reduction in PAHs was mostly attributed to the biological activities of microorganisms. The removal mechanisms include adsorption-precipitation, biodegradation and volatilization [36]. PAHs removal by volatilization was lower than 2% in conventional activated sludge process [36], while the biodegradation effect may also be minor in the absence of microbes selected for PAHs degradation [38].

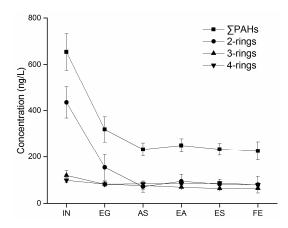


Figure 4. The variation of PAHs at different stages. Error bars represent 1 standard deviation of the mean.

3.2. PAHs in Dewatered Sludge Samples

A summary of the concentrations of PAHs in the dewatered sludge samples are shown in Table 2. All sixteen PAHs were detected in the dewatered sludge samples. Overall, the 3-ringed PAHs (184.40–351.09 ng/L) constituted the most abundant group. This was followed by the 4-ring and 6-ring groups, which together accounted for more than 32% of Σ PAHs (548.06–931.33 ng/L). Phenanthrene was the most abundant 3-ring PAH with concentration ranging from 76.88 to 135.52 ng/g.

Table 2.	Concentration	of PAHs in	dewatered	sludge	(ng/g),	soil standards	(ng/g),	and t	toxic
eguivale	nt factors.								

Ring	C1-		Dewatere	ed Sludge	So				
King Compe	Compounds	23 November	2 December	9 December	17 December	MHSPE b	RCLs c	CJ/T d	TEF a
2	NAP	76.10	51.22	45.87	41.53	15	-	-	0.001
	ANE	10.48	32.85	58.21	62.44	-	-	-	0.001
	ANA	134.88	18.80	0.34	13.52	-	-	-	0.001
3	FLU	58.81	48.74	40.28	36.22	-	-	-	0.001
	PHE	135.52	76.88	84.54	87.32	50	-	-	0.001
	ANT	11.28	7.13	4.41	2.62	50	-	-	0.01
	FLT	59.58	57.47	49.07	45.61	15	-	-	0.001
4	PYR	18.55	7.88	13.21	11.28	-	-	-	0.001
	BaA ^e	18.59	4.53	25.49	29.28	20	160	-	0.1
	CHR ^e	93.61	58.39	64.74	68.13	20	16,000	-	0.01
	BbF ^e	47.77	29.64	21.72	17.91	-	160	-	0.1
_	BkF ^e	19.24	9.87	11.60	14.11	25	1600	-	0.1
5	BaP ^e	26.06	13.37	3.56	4.88	25	16	2000	1
	DBA ^e	29.72	17.40	9.53	6.32	25	16	-	1
,	BghiP	117.91	46.79	43.54	44.13	-	-	-	0.01
6	IcdP ^e	73.23	67.69	109.94	121.87	20	160	-	0.1
\sum I	PAHs-carc	308.21	200.88	246.58	262.52	-	-	-	-
ΣL	MW PAHs	427.08	235.62	233.65	243.66	-	-	-	-
∑HMW PAHs		504.25	313.01	352.41	363.54	-	-	-	-
∑PAHs		931.33	548.64	586.06	607.20	-	-	5000	-
∑PAHs-carc/∑PAHs		33.1%	36.6%	42.1%	43.2%	-	-	-	-

^a Toxic equivalent factors [18]; ^b Soil standard in the Netherlands [9]; ^c Resident Soil in Regional Screening Levels provided by USEPA [7]; ^d Disposal of sludge from municipal wastewater treatment plant-Control standards for agricultural use (CJ/T 309-2009) [10]; ^e Carcinogenic PAHs. LMW = low molecular weight (i.e., ≤3 rings); HMW = high molecular weight (i.e., 4–6 rings); ∑PAHs-carc = the total concentration of seven carcinogenic PAHs.

The total concentration of the seven carcinogenic PAHs (i.e., \sum PAHs-carc, listed in Table 2) was 200.88 to 308.21 ng/g, accounting for 33.1 to 43.2% of \sum PAHs in dewatered sludge samples. Carcinogenic PAHs are more difficult to biodegrade due to their strong sorption to solids and hence

low bioavailability. The higher Σ PAH-carc was found in Guangdong (10 mg/kg) accounting for 33% of Σ PAHs (30 mg/kg), and other cities (average Σ PAH-carc was 7 mg/kg) accounting for 43% of average Σ PAHs (16 mg/kg), according to Cai et al. [39]. Furthermore, the concentrations of 3-rings and 4-rings were also the main contributors to Σ PAH according to Cai et al. [39] and our present study.

3.3. PAHs Source Analysis by Diagnostic Ratios

Diagnostic ratios are frequently used to identify the origins of PAHs in environmental [40,41] samples including atmospheric, aqueous, and solid phase samples [16,19,32,42]. The PAHs diagnostic ratios for raw sewage and dewatered sludge are summarized in Table 3. The interpretation of the ratios for the sewage and the sludge samples is generally ambivalent, suggesting the diversity of sources contributing to the PAHs in treatment system. For raw sewage, the light PAHs dominated (i.e., Σ LMW/ Σ HMW > 1), suggesting that the sewage PAHs may be petroleum originated [40]. The 5-ring PAH BaA/(BaA + CHR) ratio (0.67–0.69), however, points towards combustion sources. Similarly for the dewatered sludge: Σ LMW/ Σ HMW (0.66–0.85), FLT/(FLT + PYR) (0.76–0.88), and IcdP/(IcdP + BghiP) (0.38–0.73) suggest biomass burning as the origin, while ANT/(ANT + PHE) (0.03–0.08) and BaA/(BaA + CHR) (0.07–0.30) hint petroleum sources. The diagnostic ratios may be less appropriate for sewage sludge [43] as PAHs undergo redistribution through partitioning and volatilization, or are selectively enriched/eliminated through the treatment processes. Although the same may not apply to the raw sewage, upstream mixing of different sources can blur the molecular signatures of PAHs [44,45]. Overall, the apparent divergence in these ratios suggests the PAHs collected in the sewage system are likely to have different origins that include petroleum spillage/release and fossil fuel/biomass combustion.

Diagnostic Ratios	·	Dis	solved Phase	of Raw Sew	age	Dewatered Sludge			
	Main Source ^a	23 November	2 December	9 December	17 December	23 November	2 December	9 December	17 December
ΣLMW/ ΣHMW	<1 (Combustion) >1 (Petroleum)	5.14	5.86	5.33	6.13	0.85	0.75	0.66	0.67
ANT/ (ANT + PHE)	<0.1 (Petroleum) >0.1 (Combustion)	-	-	-	-	0.08	0.08	0.05	0.03
FLT/ (FLT + PYR)	<0.4 (Petroleum) 0.4–0.5 (Petroleum combustion) >0.5 (Biomass combustion)	-	-	-	-	0.76	0.88	0.79	0.80
BaA/ (BaA + CHR)	<0.2 (Petroleum) >0.35 (Combustion)	0.68	0.68	0.67	0.69	0.17	0.07	0.28	0.30
IcdP/(IcdP + BghiP)	<0.2 (Petroleum) 0.2–0.5 (Liquid fossil fuel combustion) >0.5 (Biomass combustion)	-	-	-	-	0.38	0.59	0.72	0.73

Table 3. Diagnostic ratios of selected PAHs at different samples.

Viewed from another perspective, each diagnostic ratio can be seen as identification only for its containing compounds. For example, the $\Sigma LMW/\Sigma HMW > 1$ suggests that the sewage $\Sigma PAHs$ may be petroleum originated. The 5-ring PAH BaA/(BaA + CHR) ratio (0.67–0.69) hints that the BaA and CHR may be combustion originated, but not suggests the $\Sigma PAHs$ sources. Clearly, a PAH diagnostic ratio is valid for corresponding PAHs source identification but not for whole PAHs source identification.

3.4. Risk Assessment

3.4.1. Effluent

As WWTP effluent can contribute up to 50% of the total PAHs input to the receiving water bodies, it is therefore necessary to assess the risk associated with the final effluent which would enter into

^a Adapted from Yunker et al. [40]; - One or two compounds were not detected.

a local river. Since BaP was not detectable in the effluent, the dissolved PAHs were converted to TEQ_{BaP} following equation (1) for assessment. The effluent TEQ_{BaP} ranged from 4.23 to 5.27 ng/L, which is approximately 25 times higher than the EU annual average environmental quality standard (AA-EQS = 0.17 ng/L) [7] and the tapwater screening level (3.4 ng/L) [8] proposed by US EPA, but lower than the published maximum allowable concentrations (270 ng/L in Directive 2013/39/EU and 300 ng/L in RCLs).

The personal annual health risk index of detected PAHs in the effluent was shown in Table 4. The total carcinogenic risk ranged from 1.3×10^{-5} to 1.6×10^{-5} /a with benzo(a)anthracene accounting for 99% of the total risk. This is approximately 10 to 15 times higher than the acceptable risk level of 0.1×10^{-5} /a set by Minister of Health of the People's Republic of China [46]. Although the concentrations of naphthalene were higher than benzo(a)anthracene, the risk contribution of naphthalene was considerable less as its TEQ is 100 times less than that of benzo(a)anthracene (Table 2).

	0	RfD	RefD Risk Index							
	Q	ŊD	23 November	2 December	9 December	17 December				
BaA	0.73	-	1.6×10^{-5}	1.3×10^{-5}	1.4×10^{-5}	1.3×10^{-5}				
CHR	0.0073	-	7.7×10^{-8}	6.1×10^{-8}	5.7×10^{-8}	5.1×10^{-8}				
NAP	-	0.02	9.8×10^{-10}	1.2×10^{-9}	2.4×10^{-9}	2.6×10^{-9}				
ANE	-	0.06	8.3×10^{-11}	1.0×10^{-10}	1.3×10^{-10}	1.0×10^{-10}				
ANA	-	0.06	2.1×10^{-10}	1.6×10^{-10}	1.9×10^{-10}	1.8×10^{-10}				
FLU	-	0.04	2.5×10^{-10}	2.8×10^{-10}	3.2×10^{-10}	3.2×10^{-10}				
PYR	-	0.03	7.4×10^{-10}	5.9×10^{-10}	6.4×10^{-10}	5.9×10^{-10}				

Table 4. The carcinogenic and noncarcinogenic risk index of detected PAHs in effluent.

Q = carcinogenic intensity factor; RfD = drinking reference dose of noncarcinogen.

3.4.2. Dewatered Sludge

Since only BaP and total PAHs are restricted in China, the potential health risk associated with sludge PAHs was assessed using the Netherlands soil standard [9] and the screening level recommended by US EPA [8].

PAHs in the sludge samples generally met the agricultural standard (CJ/T 309-2009) recommended by the Ministry of Housing and Urban-Rural Development of the People's Republic of China [10]. However, the sludge PAHs levels exceed the Netherlands soil standards [9] and the screening levels recommended by US EPA [8]. The sludge PAHs concentrations generally exceeded the Netherlands standards, with the indeno(1,2,3-cd)pyrene level exceeding by six-fold. When compared with the US EPA screening levels, only benzo(a)pyrene and dibenzo(a,h)anthracene levels exceeded.

For comprehensive evaluation, the TEQ_{BaP} of 16 PAHs (TEQ_{BaP16}) was calculated. The TEQ_{BaP16} ranged from 31.38 to 74.38 ng/g in sludge samples, which were 1 to 2 times of the TEQ_{BaP} of soil standard in the Netherlands ($TEQ_{BaP10} = 32.98$ ng/g). Seven carcinogenic PAHs TEQ_{BaP} ($TEQ_{BaP-carc}$) ranged from 30.20 to 72.60 ng/g accounting for 97.5 to 98.1% of TEQ_{BaP16} , which indicated that seven carcinogenic PAHs were main source of risk in sewage sludge.

4. Discussion

This work highlights the potential of employing WWTPs as the starting point for remediating/restoring water quality of surface waters in China. Studies have demonstrated that elevated PAH removal efficiencies—as high as 90 to 100%—are possible in conventional sewage treatment facilities [33,34,47]. Recent works have suggested that sewage treatment facilities may be a major contributor of PAHs to surface waters in China. Qiao et al. reported that WWTP effluent accounted for 60 to 90% of the total PAHs input to the receiving rivers within the Haihe River System [48]. Similarly, Qi et al. [49] estimated that 80% of the riverine PAHs in the greater Beijing area may be traced to sewer facilities while Zheng et al. [50] showed that the riverine PAHs levels closely follow those of the upstream WWTP effluents in the Three Gorges Reservoir region in China.

This implies WWTPs can be critical in a successful remediation and restoration of water bodies on a local or regional scale. Further investigations on the relative importance of treatment configurations, operating conditions of individual processes/units, as well as environmental factors and influent quality are needed.

5. Conclusions

The present study investigated the concentrations and removal of PAHs in a representative WWTP in Guangzhou, China. Seven PAHs (554.36–723.24 ng/L in influent; 189.64–262.73 ng/L in effluent) existed in all dissolved phase samples. Naphthalene dominated over other PAHs in the influent. All 16 US EPA PAHs (548.64–931.33 ng/g) were detected in the dewatered sludge samples, with the 3-ring PAHs as the most dominant group. The removal efficiencies of PAHs from the dissolved phase generally decreases with the number of aromatic rings. The highest removal efficiency was observed for naphthalene. Reduction in PAHs was most effective in the primary treatment phase followed by the core biological process.

Risk assessments suggested that the dissolved phase PAHs concentrations were within the maximum acceptable level while those of the dewatered sludge samples exceeded the environmental standards adopted by The Netherlands and US. Carcinogenic PAHs constitute the main source of risk in both the effluent and the sludge samples. Overall, the assessment exercise underlines the urgent need to lower carcinogenic risks associated with treated sewer and sludge.

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